



Techno-economic analysis for co-processing fast pyrolysis liquid in fossil refineries

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Agenda

- Intro to NREL
- Overview of refinery analysis
- Results of NREL-Petrobras analysis
- New refinery analysis capabilities and applications
- Questions and discussion

NREL Mission and Programs

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The National Renewable Energy Laboratory (NREL) advances the science and engineering of energy efficiency, sustainable transportation, and renewable power technologies and provides the knowledge to integrate and optimize energy systems.

| Renewable Power | Sustainable Transportation | Energy Efficiency | Energy Systems Integration |
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| | Computati | onal Science | |
| | Energy | Analysis | |
| | Energy | Storage | |
| | Materia | Is Science | |

The National Bioenergy Center (NBC) works to advance and develop innovative and costeffective solutions that move the production of biofuels, bioproducts, biochemicals, and bioenergy to market.

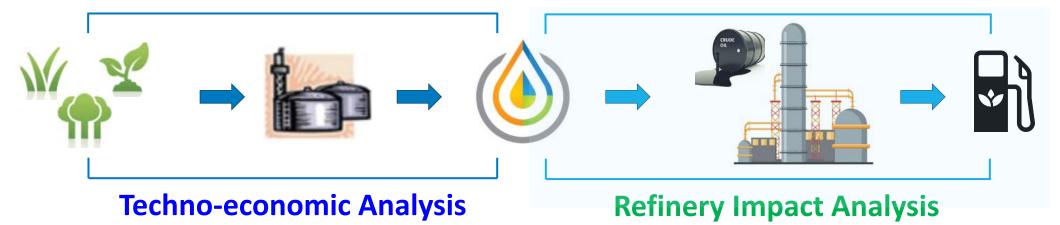
Market Analysis Sustainability, Techno-Economic,

NBC Research Areas

- Biomass Feedstocks
- Biochemical Process Development and Integration
- Biomass Deconstruction and Pretreatment
- Biogas Upgrading and Waste-to-Energy
- Biological and Catalytic Conversion of Sugars and Lignin
- Algal Biofuels
- Thermochemical Process Integration, Scale-Up, and Piloting
- Heterogeneous Catalysis for Thermochemical Conversion

Purpose of Refinery Analysis

- Leverage global refining capacity (220 billion-gal/year FCC) to reduce cost of biofuels.
- Apply an analysis approach to estimate the value of bio-blendstocks and bio-oils.
- Identify valuable properties and chemical co-products to generate market pull from refiners.
- Quantify cost and environmental impacts on refinery operations.



Quantifies production cost for bio-blendstocks

Quantifies potential bio-product value to refiners

Break-Even Value (BEV) = f (Prices, Demands, Configurations, Properties, etc.)

Difference between BEV (including policy incentives) and minimum selling price (MSP) represents the potential benefits/value for refinery and supply chain.

History of NREL Refinery Analysis

2010 – 2014: National Advanced Biofuels Consortium

- Property comparisons of bio- and fossil- intermediates
- Initial biofuels blending model in Aspen PIMS





2014 – 2017: NREL-Petrobras Co-Processing Analysis

 Fluid Catalytic Cracking (FCC) and product finishing yield models coupled with economics for initial optimization capabilities.

2016 – 2021: Co-Optima Refinery Analysis (collaboration with PNNL and ANL)

- Complete refinery models with various configurations quantify values of bioblendstocks and bio-intermediates.
- Tools integrated with Aspen Plus quantify environmental benefits.
- Refinery models are now capable of direct blending bio-blendstocks and coprocessing bio-intermediates via hydroprocessing and FCC.

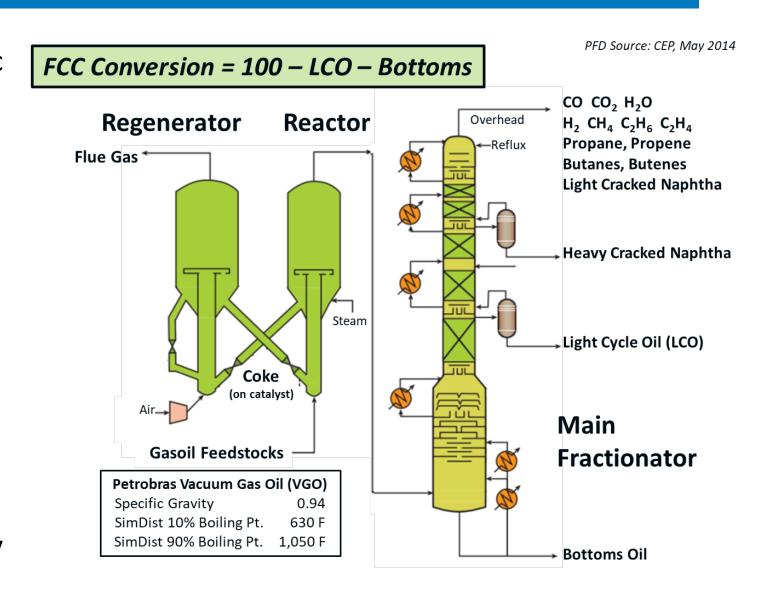


NREL-Petrobras FCC Co-Processing Analysis

Assess the technical and economic feasibility of co-processing raw, biomass-derived pyrolysis oil with fossil feedstocks in FCC to produce renewable hydrocarbon fuels and chemicals.

Leverage existing FCC capacity to reduce economic risk of biofuels production.

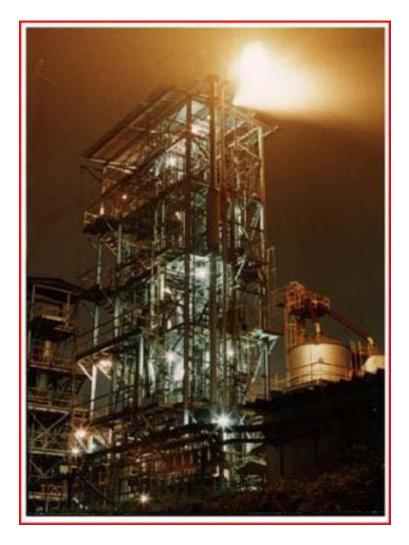
- 90-billion gallons/year in US
- 220-billion gallons/year globally



Petrobras FCC Co-Processing Experiments

Petrobras "SIX" demo unit has same hardware as a commercial FCC

- Feed nozzles
- Riser cyclone
- Packed stripper
- Heat balanced
- Mass flowrate: 200 kg/h
- Riser: L=18 m



Co-Processing Experiments

- Two pine-derived pyrolysis oils with consistent physical properties
- Mass balance range of 96 100%
- 3-hour test runs
- Cumulative time w/ py-oil > 400 hours
- Up to 20 wt% pyrolysis oil in FCC feed
- 54 experimental data points

Fuel Processing Technology 131 (2015) 159-166

Co-processing raw bio-oil and gasoil in an FCC Unit

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a PETROBRAS, Centro de Pesquisas e Desenvolvimento Leopoldo A. Miguez de Mello (CENPES), Ilha do Fundão, Av. Horácio Macedo, 950, Rio de Janeiro, R.J. Brazil

Fuel 188 (2017) 462-473

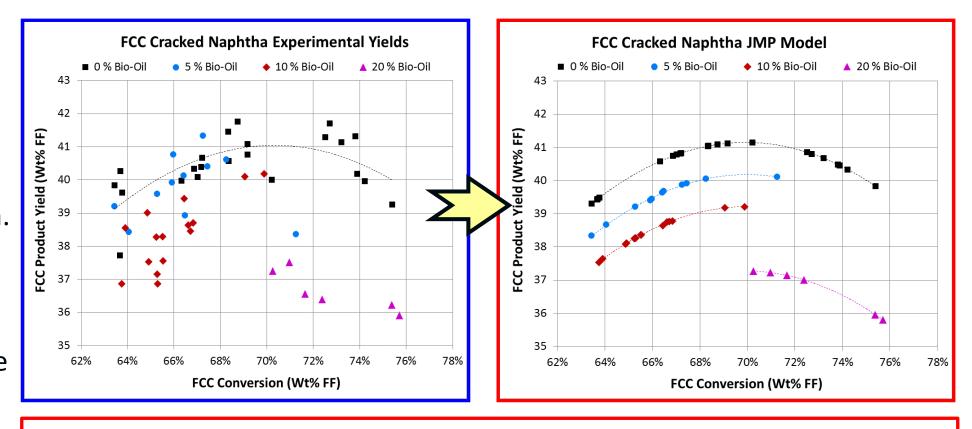
Fast pyrolysis oil from pinewood chips co-processing with vacuum gas oil in an FCC unit for second generation fuel production

Andrea de Rezende Pinho a.*, Marlon B.B. de Almeida a, Fabio Leal Mendes a, Luiz Carlos Casavechia b, Michael S. Talmadge c, Christopher M. Kinchin , Helena L. Chum C

^a PETROBRAS, Centro de Pesquisas e Desenvolvimento Leopoldo A. Miguez de Mello (CENPES), Ilha do Fundão, Av. Horácio Macedo, 950, Rio de

NREL-Petrobras Yield Model from Experimental Data

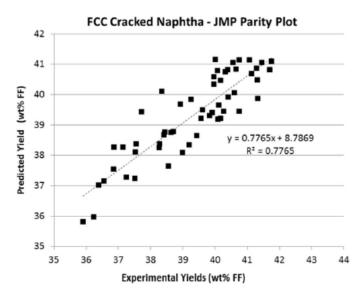
- Utilized statistical software package to derive yield models from experimental data.
- Yield models, combined with economics, enable optimizations to identify most profitable operating points.

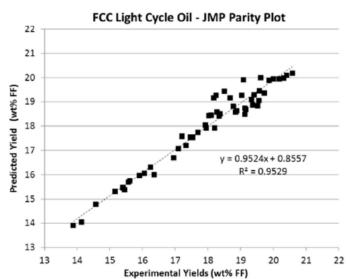


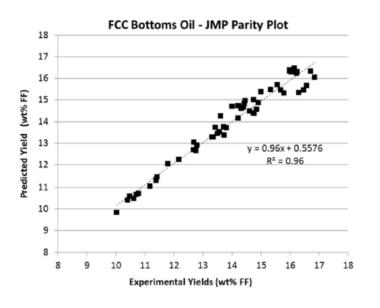
| Complete | Oxygen Species | Refinery Fuels | LPG Products | Liquid Products |
|-----------|--------------------------|----------------------------|-------------------|-----------------------|
| FCC Yield | CO CO ₂ Water | Dry Gas (C ₂ -) | Propane Propylene | Cracked Naphtha |
| | | Coke | i-Butane n-Butane | Light Cycle Oil (LCO) |
| Model | | | Butenes | Bottoms Fuel Oil |

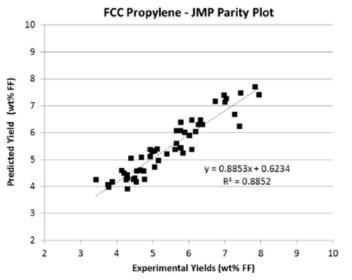
Yield Model Validations with Experimental Data

- Validated yield model predictions for all raw products from FCC unit.
- Utilized Aspen HYSYS model to further validate model predictions as a function of FCC reactor severity.



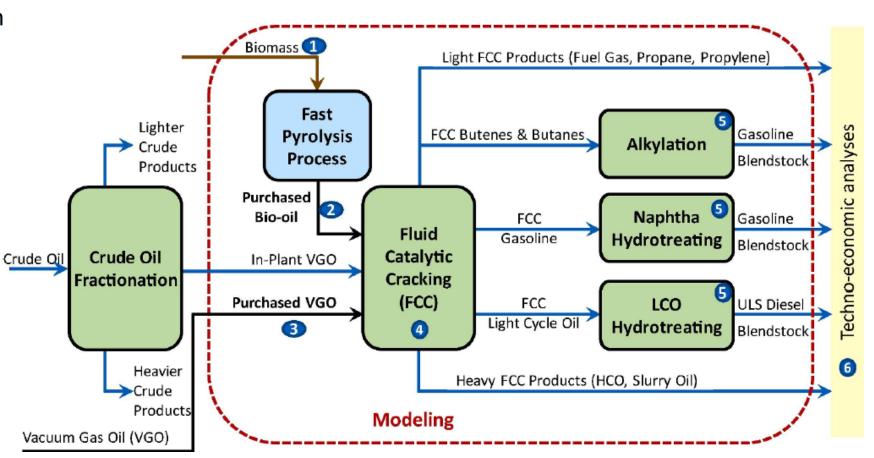






Scope of NREL-Petrobras Analysis

- Scope includes downstream product upgrading units for finished blendstocks:
 - i-C₄ and C₄-olefins converted to high-octane gasoline blendstock via alkylation.
 - Cracked naphtha hydrotreating to gasoline blendstock.
 - LCO hydrotreating to ULSD blendstock.



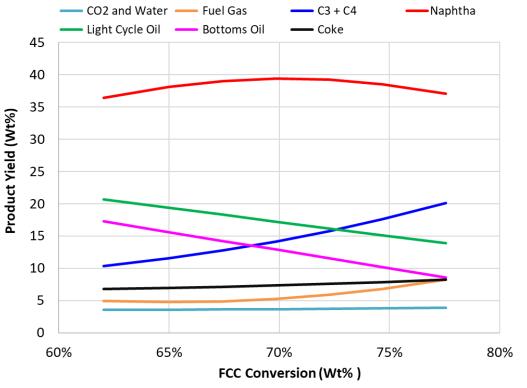
Enabling Optimization with Yield and Pricing Models

- Add product pricing model to convert complex FCC yields to single value (\$/unit FCC feed)
- Profit = value of products minus
 - -Cost of feeds
 - Costs of catalysts,utilities, H₂,royalties
 - Amortized capex

Refinery Process Yield Model





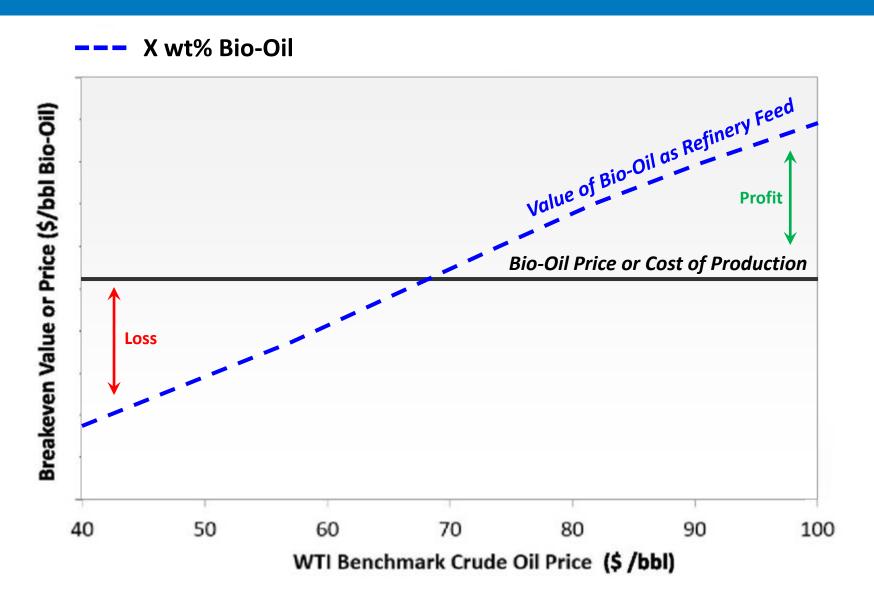


West Texas Intermediate (WTI) 80 (\$/BBL)

| Products | Price | Unit |
|-----------------------------------|--------|--------|
| Natural Gas | 0.1195 | \$/LB |
| Propane | 0.9979 | \$/GAL |
| Propylene | 2.2232 | \$/GAL |
| n-Butane | 1.2233 | \$/GAL |
| i-Butane | 1.2998 | \$/GAL |
| Conventional Regular Gasoline | 2.2661 | \$/GAL |
| Conventional Midgrade Gasoline | 2.3501 | \$/GAL |
| Conventional Premium Gasoline | 2.5619 | |
| Reformulated Regular Gasoline | 2.3669 | \$/GAL |
| Reformulated Midgrade Gasoline | 2.5061 | \$/GAL |
| Reformulated Premium Gasoline | 4.0000 | \$/GAL |
| Alkylate Intermediate | 2.5617 | \$/GAL |
| Jet Fuel | 2.4149 | \$/GAL |
| Ultra Low Diesel Fuel (ULSD) | 2.4193 | \$/GAL |
| California Diesel Fuel (CDF) | 2.0000 | \$/GAL |
| Heating (No 2) Oil | 2.3891 | \$/GAL |
| Light Cycle Oil (LCO) | 2.3916 | \$/GAL |
| Vacuum Gas Oil (VGO) | 2.2587 | \$/GAL |
| Residual (No 6) Oil - 0.3% Sulfur | 1.3910 | \$/GAL |
| Residual (No 6) Oil - 1% Sulfur | 1.0540 | \$/GAL |
| Residual (No 6) Oil - 3% Sulfur | 0.7574 | \$/GAL |
| | | |

Illustrative Example for Presentation of Results

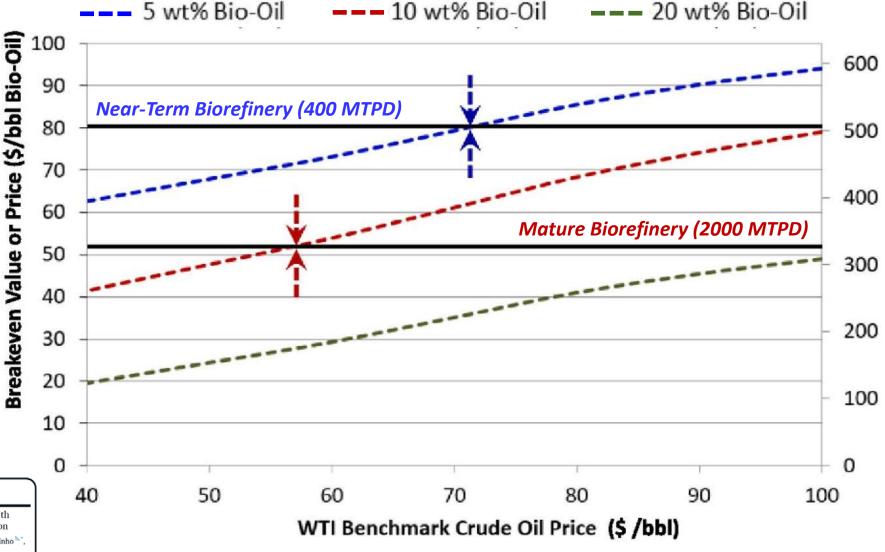
- Dark, solid lines represent costs of bio-oil production at different biorefinery scales.
- Colorful, dotted lines represent the values of bio-oil as refinery (FCC) feedstock.



Breakeven Value for Fast Pyrolysis Oil Co-Processing

Breakeven Analysis

- Revenue equals cost at "Breakeven Point"
- "Pyrolysis Oil Breakeven Value" = f(value of products)
- Profit realized when cost < "Breakeven Value"



Fuel 293 (2021) 119960

Techno-economic analysis for co-processing fast pyrolysis liquid with vacuum gasoil in FCC units for second-generation biofuel production

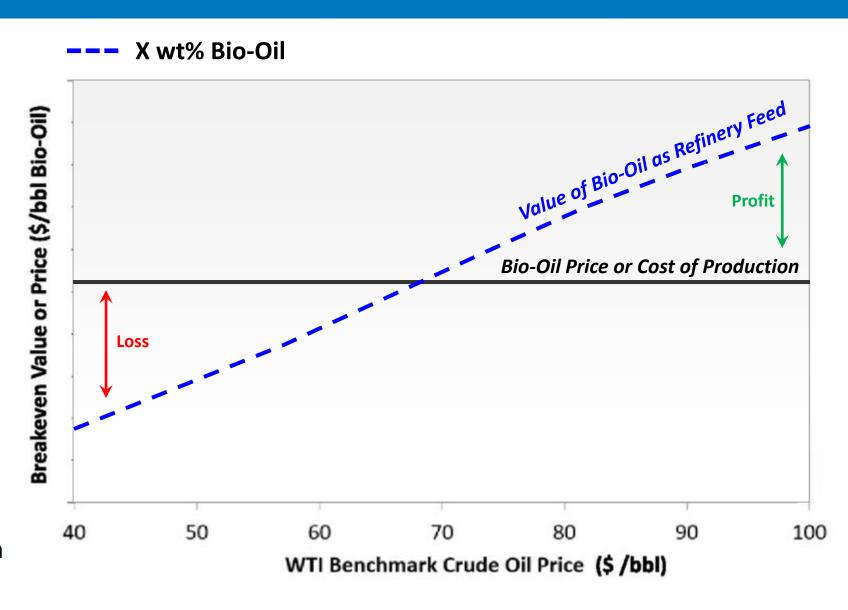
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Breakeven Value or Price (\$/

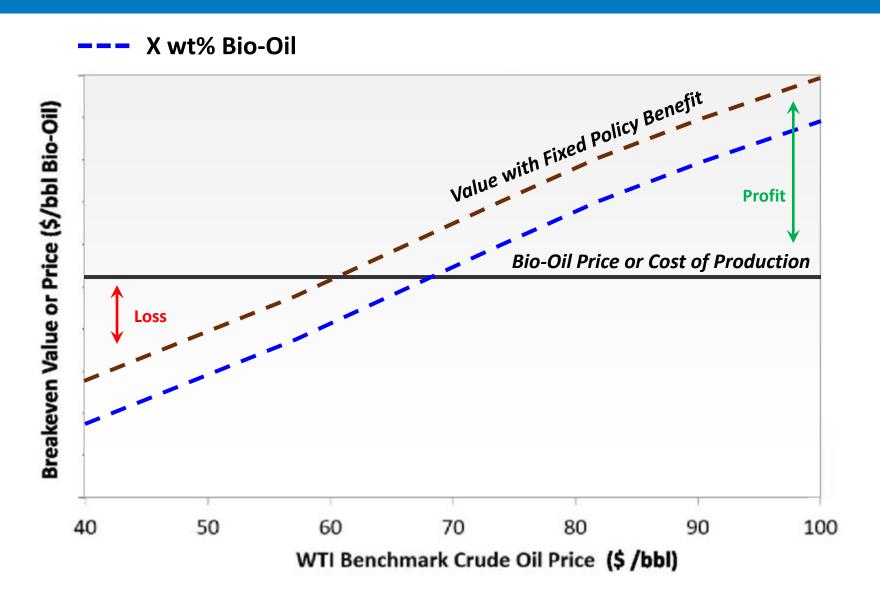
Policy Insights with Illustrative Example

- Biomass and derivative prices are NOT tied to crude prices.
- Refineries have high level of risk due to uncertainty in product market prices.
- Future tech
 development will
 increase value and
 decrease cost.
- Refiners need policy help in near-term when market values are low.



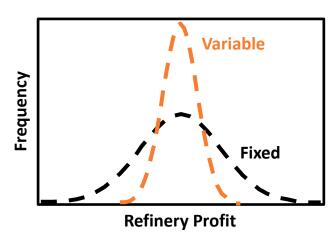
Policy Insights with Illustrative Example

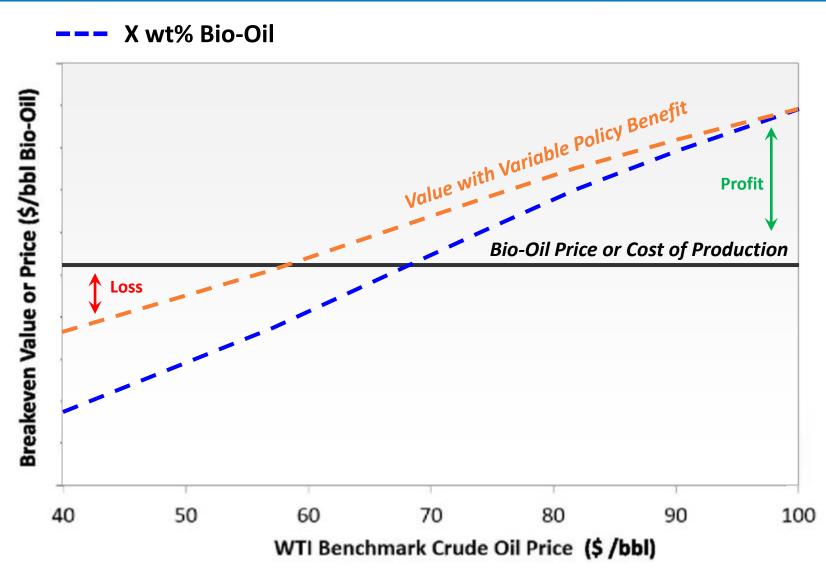
- Fixed-value policy may be relatively costly for taxpayer/consumer.
- Risk of economic loss may remain substantial.



Policy Insights with Illustrative Example

- Variable policy
 may reduce risk of
 economic loss
 while minimizing
 excessive profit.
- Modeled results show impact on risk probability.





Overview of Refinery Analysis with Aspen PIMS



Refinery configuration and unit capacity basis from EIA.



Bio-blendstock/-intermediate cost, props, yields from TEA.

ASTM

ASTM fuel specifications consistent with industry.



Crude and product pricing data from OPIS and PRISM.



Market projections from EIA, OPIS, ADOPT.



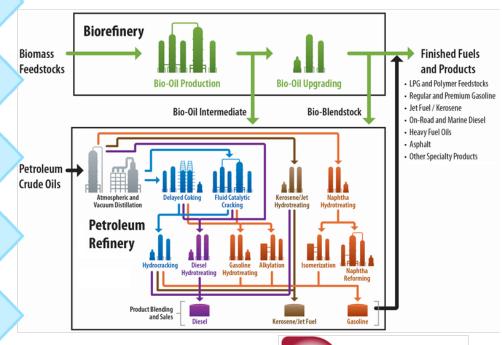
ADOPT

Refinery capital investment basis from published sources.



Direct industry input through several on-going projects.

Biorefinery Models



Aspen PIMS Refinery Models in By AspenTech Integrated with Bioeconomy R&D needs via LCA calculations. Optimizations. data gaps.

Outputs:

- Complete operational and economic profiles for optimized refinery solutions.
- Valuations of biofeedstocks.
- Effective policy designs to de-risk biofuels production in refineries.
- Basis for US refinery network of "metamodels" for bioeconomy modeling.

Davison Circulating Riser (DCR) for Co-Processing

Evaluate FCC co-processing strategies by feeding CFP oils or other biogenic materials (FOGs, waxes) with VGO into the riser to produce BC-containing fuels

Key System Specifications – DCR for Co-processing

Feed Type: Liquids

Feed Rate: 1.2 kg/hr

Catalyst Type and Form Factor/Size: Refinery-type, zeolite-based,

fluidizable (FCC), 80-100 micron.

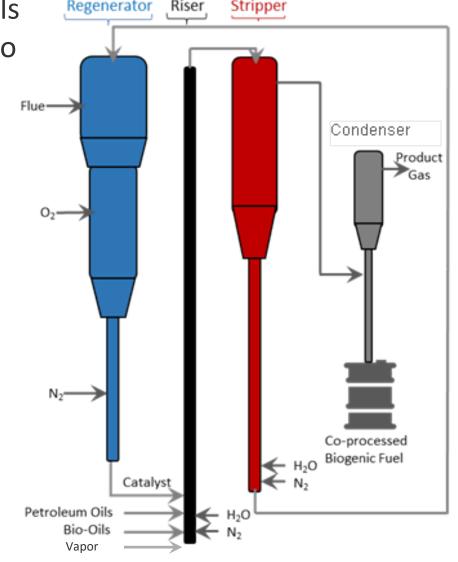
Catalyst Charge/Feed Rate: 1.8 kg, circulation rate 7-10 kg/hr

Operating Temperature Range: 475-550°C

Operating Pressure Range: 2-2.6 bar

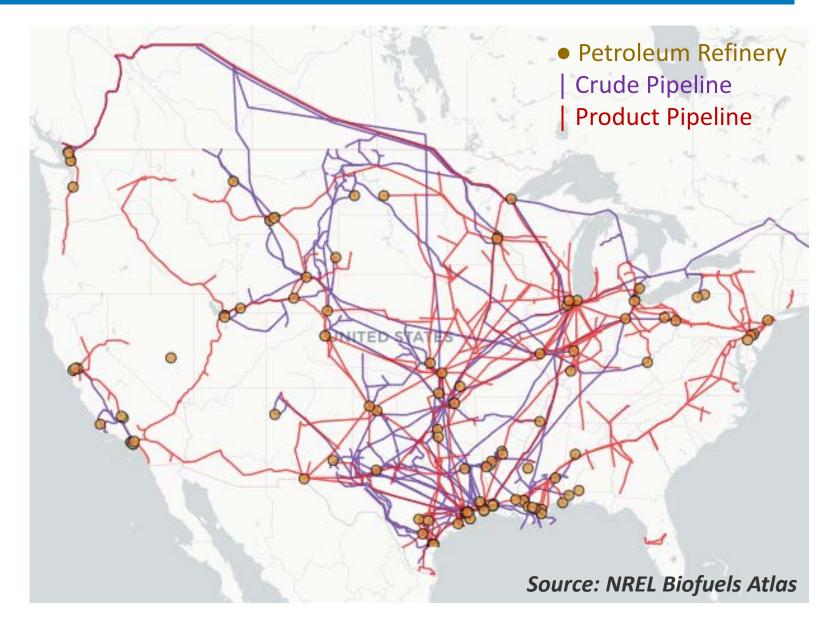
Reactor Configuration(s): Riser reactor + stripper + regenerator

Additional Specifications: Catalyst recirculated for stripping (HC removal) and regeneration (coke removal). DCR mimics FCC refinery operations by cracking large molecules to fuel-range molecules.



Future Goals for Refinery Analysis

- Identify low-carbon and low-cost strategies for renewable fuels and chemicals that leverage existing refineries.
- Continue to collaborate with industry partners on commercializing attractive business cases.
- Inform effective policy designs with modeled results.



Developing New Modeling Capabilities

- Integrate emerging technologies (and feedstocks) for bio-oil production
- Catalytic fast pyrolysis
 Hydropyrolysis
 Hydrothermal liquefaction
- Develop analysis for renewable olefins and aromatics from refineries
- Integrate environmental calculations for multi-objective optimizations (ANL)
- Explore alternative integration points
- Hydroprocessing (PNNL/NREL)
 Residuum Fluid Cat Cracking (RFCC)

- Delayed Coker
- Fluid/Flexi-CokerMarine Fuels
- Utilize refinery models in bioeconomy resource optimizations

Source Publications

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Thank you! Questions?

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